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## Analysis of the nitrogen adsorption technique to characterize porous materials

Error analysis guides the way



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Engineering [www.cheme.nl/ce](http://www.cheme.nl/ce)

M.F. de Lange, T.J.H. Vlugt, J. Gascon, F. Kapteijn, *Micropor Mesopor Materials* 200 (2014) 199–215



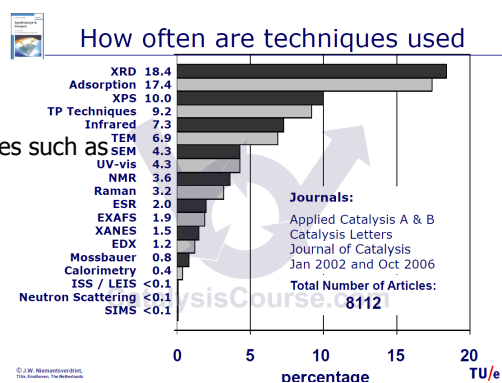
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## Introduction

### Adsorptive characterization $N_2$ @ 77 K

- One of most used tools for characterization of
  - Catalysts
  - Porous adsorbents

- Physical adsorption yields quantities such as
  - Pore volume
  - Specific surface area
  - Pore size distribution



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## What's the matter?

Reported values not always

- Reproducible
- Physically sound
- Statistically correct

### MIL-101(Cr)

**Table 1.** N<sub>2</sub> Adsorption properties hydrogen uptake capacities in air its composite at 77 K

Sample	BET surface area (m <sup>2</sup> ·g <sup>-1</sup> )	Por. volun (cm <sup>3</sup> ·g <sup>-1</sup> )
MIL-101	2887.39	1.41
AC@MIL	3555.61	1.71
101/A	2767.93	1.41
AC@MIL	2402.67	1.11
101/C	1856.35	0.90
101/D	946.96	0.41
Activated carbon		

BET, Brunauer-Emmett-Teller.

constant = 91.759

57.012 nm  
57.012 nm  
0.376 nm

1.14676 cm<sup>3</sup>/g  
12.762 m<sup>3</sup>/g  
3201.206 m<sup>3</sup>/g

**Accuracy – uncertainty Guidelines**

de Lange et al., *Micropor Mesopor Materials* 200 (2014) 199–215

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## Volumetric technique

- Dosing N<sub>2</sub> gas  $p_{man}$   $V_{man}$   $T$
- Apply Gas law  $\frac{pV}{RT} = z \cdot n$
- 'Missing' amount adsorbed

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## Error propagation analysis

$$\sigma_y^2 = \sum \left( \frac{\partial y}{\partial x_i} \right)^2 \sigma_{x_i}^2$$

- Volumes determination

e.g. see J.R. Taylor

$$V_{cell} = \left( \frac{p_{man}^0 - p_{man}^1}{p_{cell}^1 - p_{cell}^0} \right) V_{man}$$

$$\sigma_{V_{cell}}^2 = \left( \frac{1}{p_{cell}^1 - p_{cell}^0} V_{man} \right)^2 (2\sigma_p^2) + \left( \frac{p_{man}^0 - p_{man}^1}{(p_{cell}^1 - p_{cell}^0)^2} V_{man} \right)^2 (2\sigma_p^2) + \left( \frac{p_{man}^0 - p_{man}^1}{p_{cell}^1 - p_{cell}^0} \right)^2 \sigma_{V_{man}}^2$$

$V_{cold} = V_{cell} - V_{warm}$ 

$$\sigma_{V_{cold}}^2 = \sigma_{V_{cell}}^2 + \sigma_{V_{warm}}^2$$

$$V_{warm} = \left( \frac{\frac{p_{cell}^0}{p_{cell}^1} - \frac{T_{warm}}{T_{cold}}}{1 - \frac{T_{warm}}{T_{cold}}} \right) V_{cell}$$

$$\sigma_{V_{warm}}^2 = \left( \frac{1}{p_{cell}^1 \left( 1 - \frac{T_{warm}}{T_{cold}} \right)} V_{cell} \right)^2 \sigma_p^2 + \left( \frac{\frac{p_{cell}^0}{p_{cell}^1} - \frac{T_{warm}}{T_{cold}}}{1 - \frac{T_{warm}}{T_{cold}}} V_{cell} \right)^2 \sigma_p^2 + \left( \frac{T_{cold} (p_{cell}^0 - p_{cell}^1)}{p_{cell}^1 (T_{warm} - T_{cold})} V_{cell} \right)^2 \sigma_{T_{warm}}^2 + \left( \frac{T_{warm} (p_{cell}^0 - p_{cell}^1)}{p_{cell}^1 (T_{warm} - T_{cold})} V_{cell} \right)^2 \sigma_{T_{cold}}^2 + \left( \frac{p_{cell}^0 - T_{warm}}{1 - \frac{T_{warm}}{T_{cold}}} \right)^2 \sigma_{V_{cell}}^2$$

J.R. Taylor, An introduction to Error Analysis, 2nd ed., University Science Books, 1997. Catalysis Engineering – ChemE 5

## Error propagation analysis

$$\sigma_y^2 = \sum \left( \frac{\partial y}{\partial x_i} \right)^2 \sigma_{x_i}^2$$

- e.g. see J.R. Taylor

$$n_{dosed}(i) = \left( \frac{p_{man}^0(i) - p_{man}^1(i)}{RT_{warm}} \right) V_{man}$$

$$\sigma_{n_{dosed}}^2(i) = \left( \frac{V_{man}}{RT_{warm}} \right)^2 2\sigma_p^2 + \left( \frac{\Delta p_{man}(i)}{R(T_{warm})^2} V_{man} \right)^2 \sigma_{T_{warm}}^2 + \left( \frac{\Delta p_{man}(i)}{RT_{warm}} \right)^2 \sigma_{V_{man}}^2$$

$n_{ads}(i) = n_{dosed}(i) - n_{gas}(i) + n_{ads}(i-1)$ 

$$\sigma_{n_{ads}}^2(i) = \sigma_{n_{gas}}^2(i) + \sigma_{n_{dosed}}^2(i) + \sigma_{n_{ads}}^2(i-1)$$

$$n_{gas}(i) = p_{cell}^i \left( \frac{V_{warm}}{RT_{warm}} + \frac{V_{cold}}{Z(p_{cell}^i)RT_{cold}} \right)$$

$$\sigma_{n_{gas}}^2(i) = \left( \frac{V_{warm}}{RT_{warm}} + \frac{V_{cold}}{RT_{cold} Z(p_{cell}^i)} + \frac{p_{cell}^i \alpha(T) V_{cold}}{RT_{cold} (Z(p_{cell}^i))^2} \right)^2 \sigma_p^2 + \left( \frac{p_{cell}^i}{RT_{warm}} \right)^2 \sigma_{V_{warm}}^2 + \left( \frac{p_{cell}^i V_{warm}}{R(T_{warm})^2} \right)^2 \sigma_{T_{warm}}^2 + \left( \frac{p_{cell}^i}{Z(p_{cell}^i) RT_{cold}} \right)^2 \sigma_{V_{cold}}^2 + \left( \frac{p_{cell}^i V_{cold}}{Z(p_{cell}^i) R(T_{cold})^2} \right)^2 \sigma_{T_{cold}}^2$$

error accumulation

J.R. Taylor, An introduction to Error Analysis, 2nd ed., University Science Books, 1997. Catalysis Engineering – ChemE 6

## Measurements & procedures

**Materials:**

- MIL-101(Cr)
- UiO-66
- Norit RB2
- $\gamma$ -alumina (CK-300)
- Sigma-1

**Autosorb 6B**

**Error propagation:**

$$\sigma_y^2 = \sum \left( \frac{\partial y}{\partial x_i} \right)^2 \sigma_{x_i}^2$$

**Pore volume (Gurvich)**

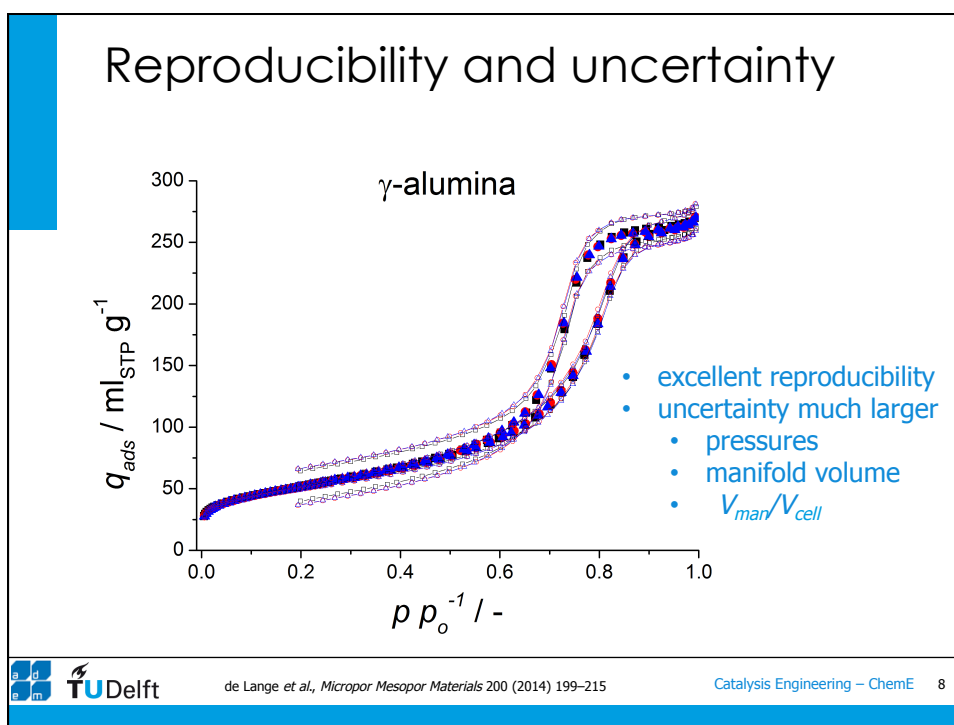
**Surface area (BET)**

**Pore size distr. (BJH)**

Uncertainty in adsorption measurement  
[ $\sigma_{qads}^2$ ]

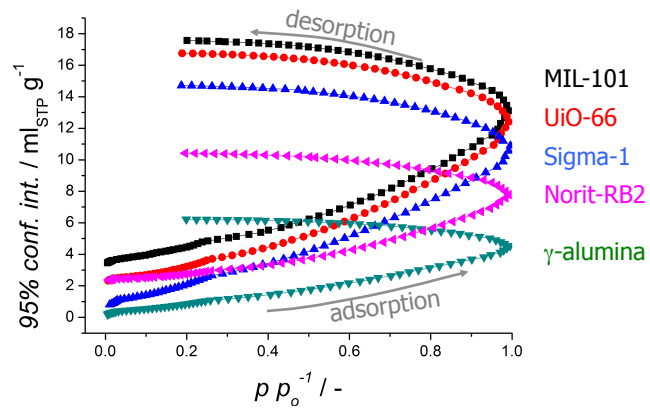
3x

TU Delft de Lange et al., *Micropor Mesopor Materials* 200 (2014) 199–215 Catalysis Engineering – ChemE 7



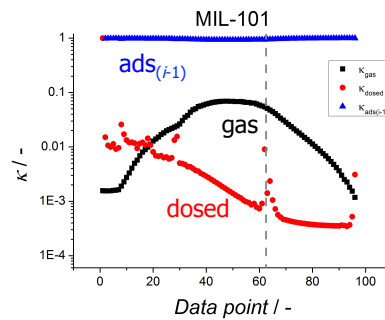
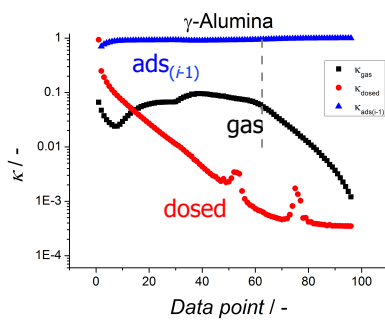
## Uncertainties - 95% confidence interval

(single dose assumption)



## Error breakdown

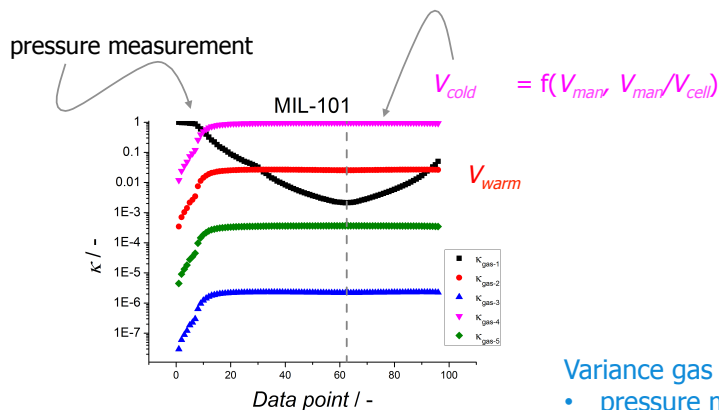
$$n_{ads}(i) = n_{dosed}(i) - n_{gas}(i) + n_{ads}(i-1)$$



Variance (normalized) of gas, dose, adsorbed (i-1)  
Single dose assumption

Variance adsorbed amount previous step largest

## Error breakdown - variance $ads_{(i-1)}$

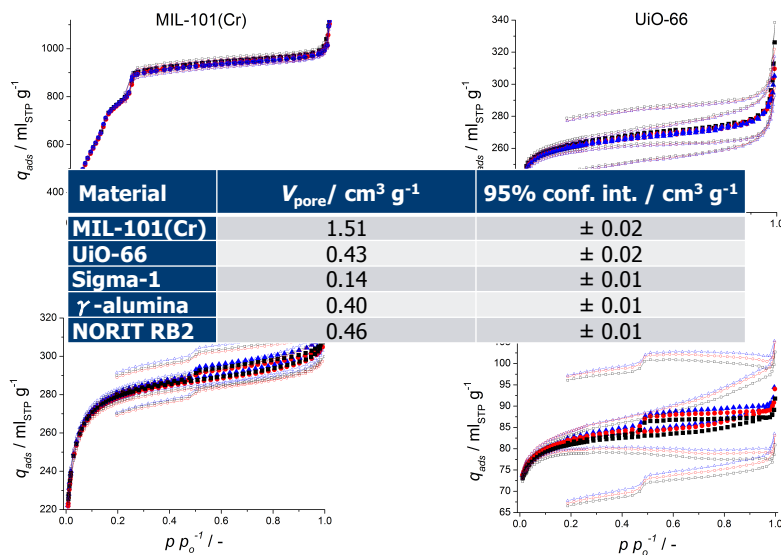


Variance adsorbed arises mainly from gas phase variance  
Single dose assumption

Variance gas phase amount:

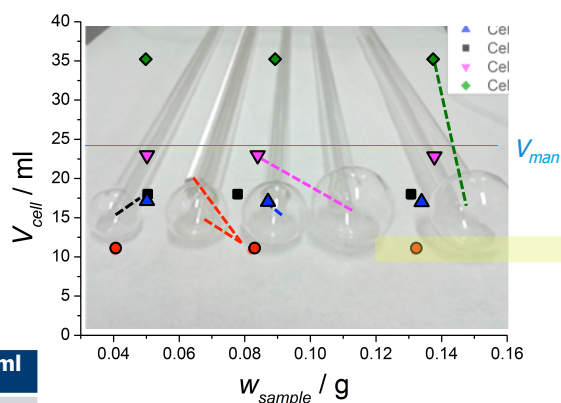
- pressure measurement
- manifold volume
- $V_{man}/V_{cell}$

## Reproducibility and uncertainty



## Sample amount and cell volume

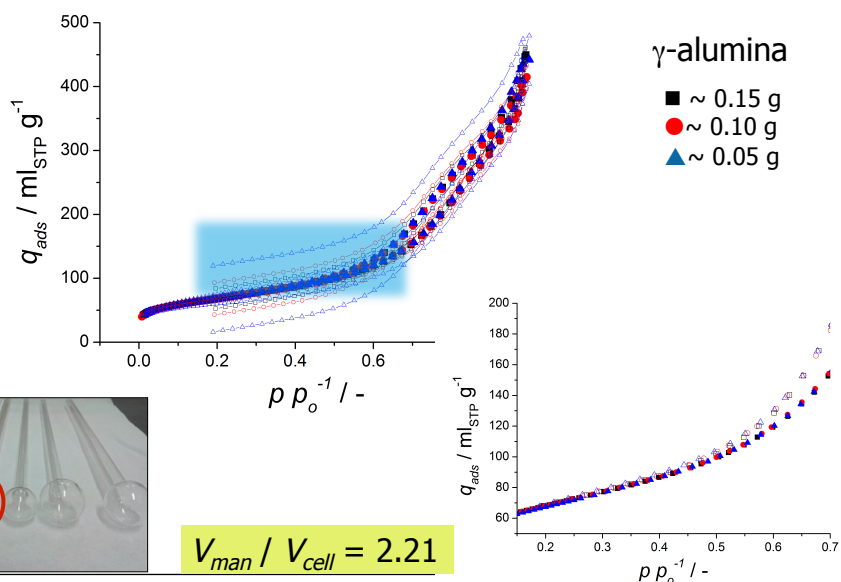
$\gamma$ -alumina (000-3P)  
(mesoporous)

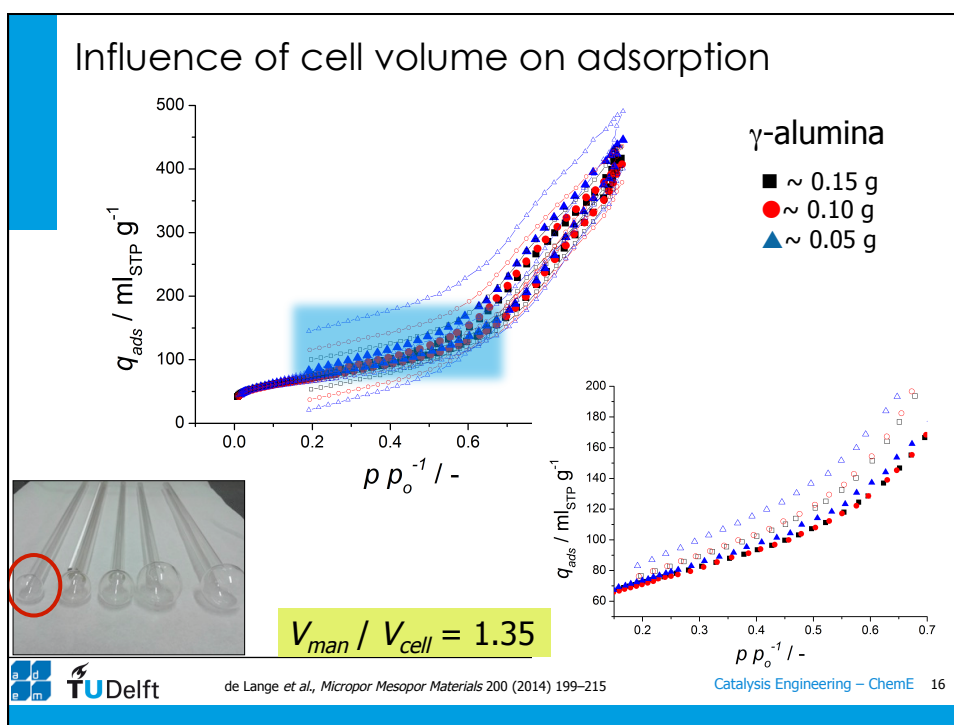
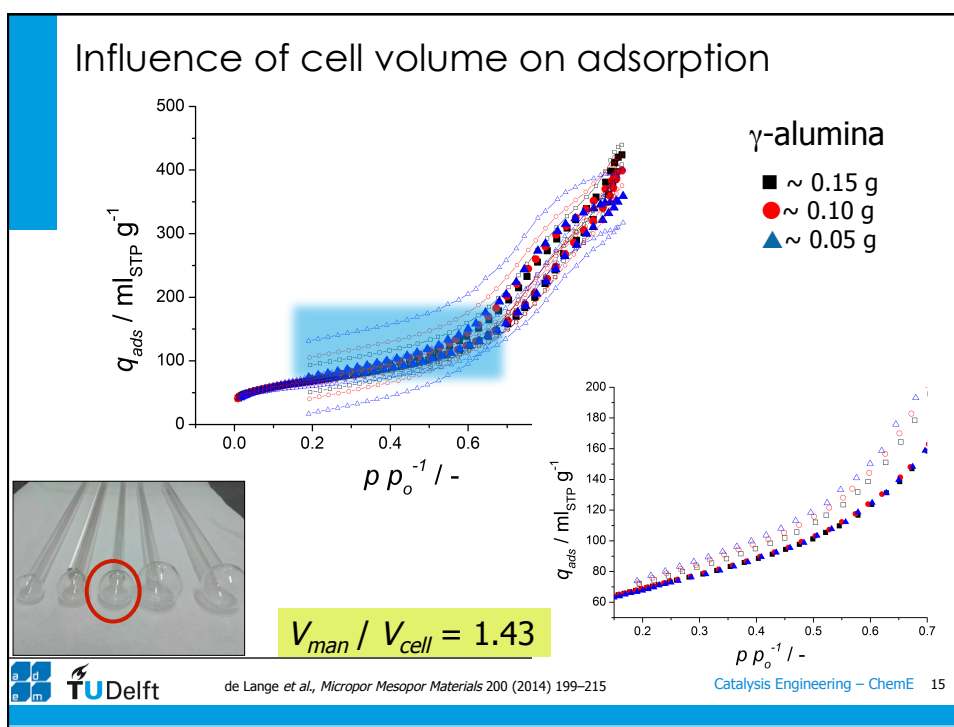


Material	$w_{\text{sample}} / \text{g}$	$V_{\text{cell}} / \text{ml}$
MIL-101(Cr)	0.12	10.5
UiO-66	0.13	11.0
Sigma-1	0.15	11.1
$\gamma$ -alumina	0.18	10.8
NORIT RB2	0.20	10.7

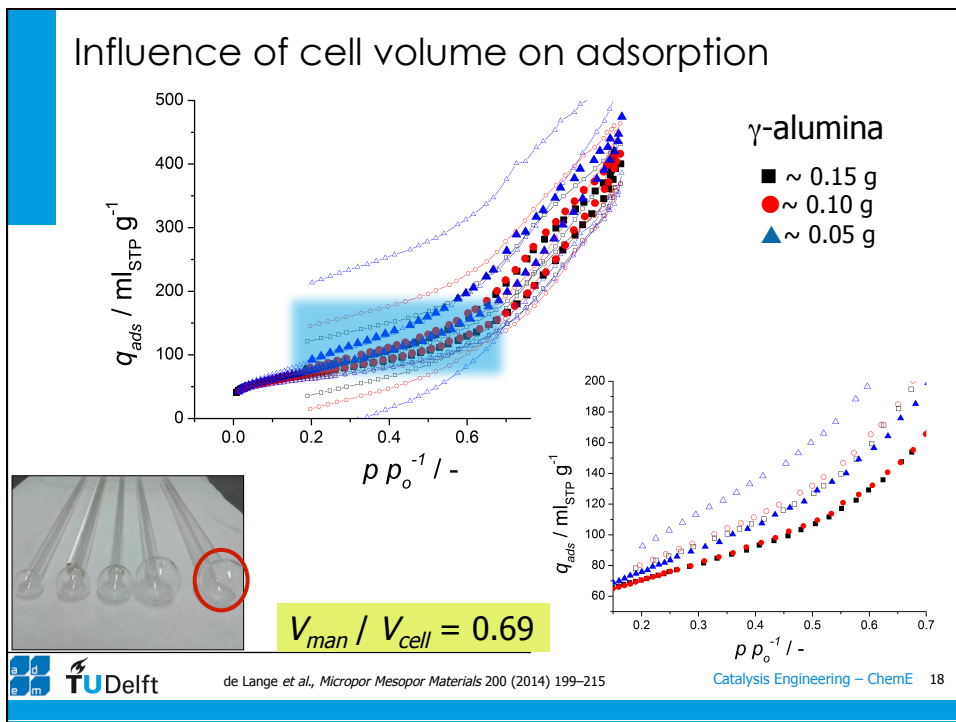
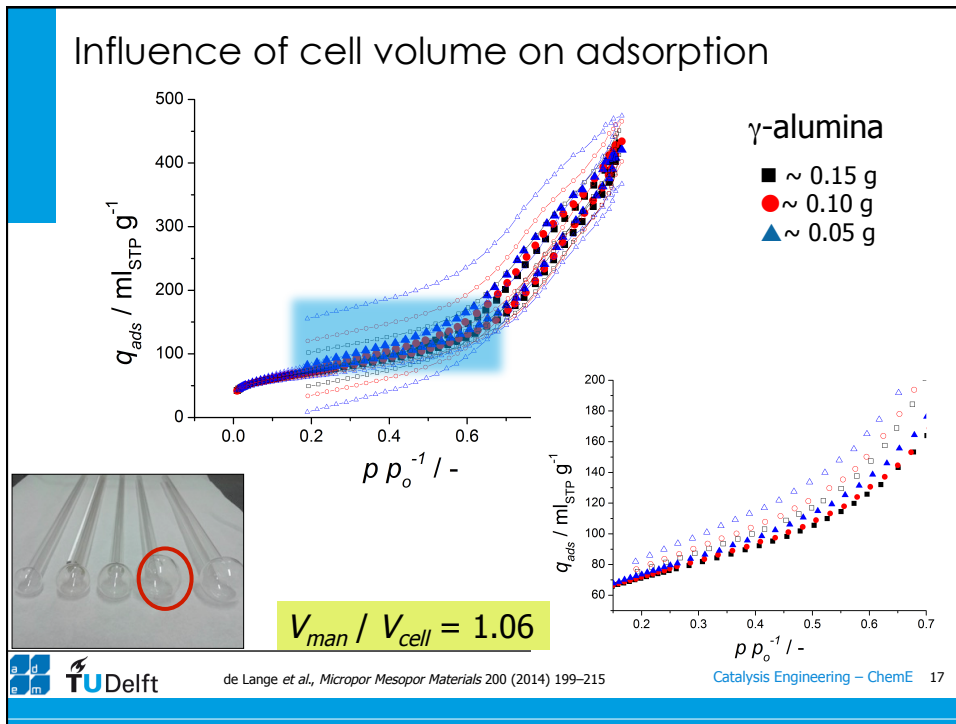
Variation ratio  $V_{\text{man}}/V_{\text{cell}}$

## Influence of cell volume on adsorption







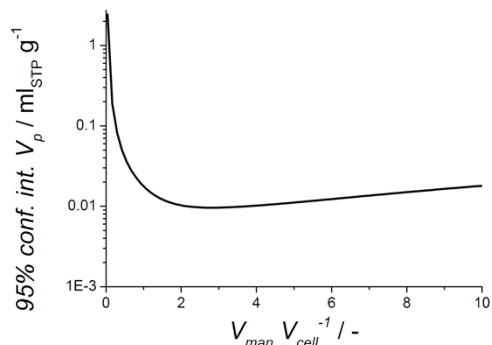


### Optimum $V_{man} / V_{cell}$ for minimal uncertainty?

Simulations using Langmuir isotherm

Effect on  $V_p$

$$q = q_m \left( \frac{K \frac{p}{p_o}}{1 + K \frac{p}{p_o}} \right)$$



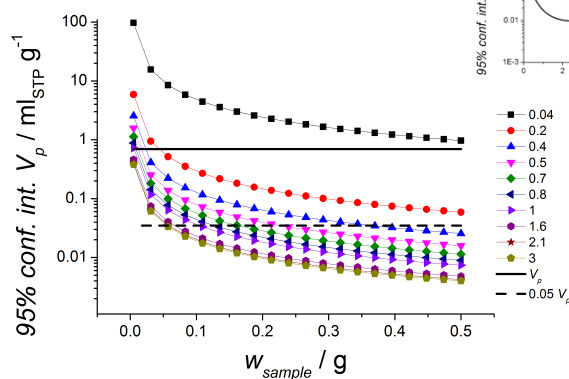
$q_m = 500 \text{ ml}_{\text{STP}} \text{ g}^{-1}$   
 $K = 10 \text{ bar}^{-1}$   
 $w_{\text{sample}} = 0.2 \text{ g}$   
 $p/p_o = 0.9$

Optimum at  $V_{man}/V_{cell}$  ratio  $\sim 2-3$

### Optimum $V_{man} / V_{cell}$ for minimal uncertainty?

Variation sample size

Effect on  $V_p$

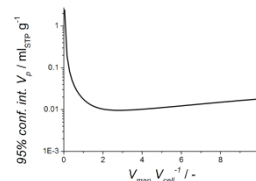
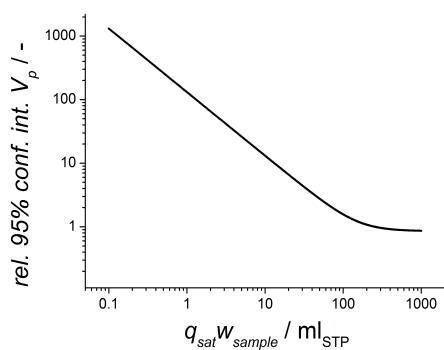


- Improves for larger samples
- Minimum at ratio  $\sim 2-3$

## Optimum $V_{man} / V_{cell}$ for minimal uncertainty?

Variation sample mass

Effect on  $V_p$



Optimum reached at sorbed amounts of  $\sim 100 \text{ ml}_{\text{STP}}$

## Observations – Variation sample mass and cell volume

Effect on  $V_p$

- Optimum ratio  $V_{man}/V_{cel} \sim 2-3$
- Artificial hysteresis introduced for
  - Larger cell volume
  - Lower sample mass (+ higher inaccuracy)
- Sorbed capacity  $\sim 100 \text{ ml}$

## BET model and surface area

$$q = q_m \left( \frac{C \left( \frac{p}{p_o} \right)}{\left\{ 1 - \frac{p}{p_o} + C \left( \frac{p}{p_o} \right) \right\} \cdot \left\{ 1 - \left( \frac{p}{p_o} \right) \right\}} \right)$$

$$\frac{\frac{p}{p_o}}{q \left( 1 - \frac{p}{p_o} \right)} = \left( \frac{1}{Cq} \right) + \left( \frac{C-1}{Ca} \right) \cdot \left( \frac{p}{p_o} \right)$$

$$q_m = \left( \frac{1}{I+S} \right)$$

- Traditionally equation is **linearized**:

- Linear least squares fitting procedure
- Quality visible "by the eye"
- Applicable somewhere between:
  - 0.05–0.35  $p/p_o$  (B,E & T)
  - 0.05–0.30  $p/p_o$  (IUPAC)

Important:

-Values highly determined by fitting strategy-

- $C > 0$
- Choose right  $p/p_o$  window

$$S_{BET} = \frac{q_m \rho_{STP}^{vap} N_A A_{CS}}{M_{N_2}}$$

Determination limits  $p/p_o$   
Direct fitting (non-linear parameter estimation)



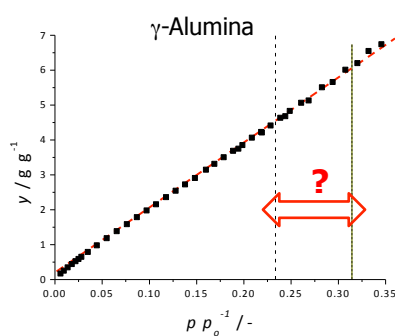
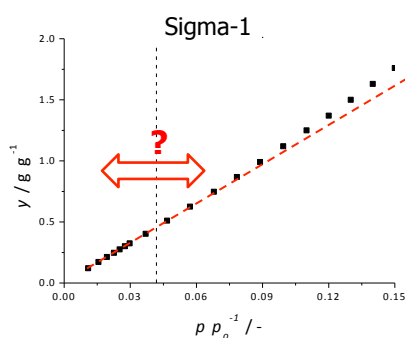
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Brunauer, Emmett & Teller, 1938

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## Linearized BET

- Linearization changes error distribution
- What tells your 'eye'?



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